

STIC Search Report

STIC Database Tracking Number 2015

TO: Tony S Chuo

Location: REM 6C11

Art Unit: 1745 May 24, 2007

Case Serial Number: 10/664818

From: Mei Huang Location: EIC 1700

REMSEN 4B28

Phone: 571/272-3952 Mei.huang@uspto.gov

Search Notes

Examiner Chuo,

Please feel free to contact me if you have any questions or if you would like to refine the search query.

Thank you for using STIC search services!

Regards, Mei Huang





STIC Search Results Feedback Form

-		CONTRACT.		
	I al.	-	414	TA
-		57 E	7 I E	I #
		X A	4	

Questions about the scope or the results of the search? Contact the EIC searcher or contact:

Kathleen Fuller, EIC 1700 Team Leader 571/272-2505 REMSEN 4B28

 I am an examiner in Workgroup: Example: 1713 Relevant prior art found, search results used as follows:
102 rejection
103 rejection
Cited as being of interest.
Helped examiner better understand the invention.
Helped examiner better understand the state of the art in their technology.
Types of relevant prior art found:
☐ Foreign Patent(s)
 Non-Patent Literature (journal articles, conference proceedings, new product announcements etc.)
> Relevant prior art not found:
Results verified the lack of relevant prior art (helped determine patentability).
Results were not useful in determining patentability or understanding the invention.
Comments:

Banks, Kendra

From:

TONY CHUO [Tony.Chuo@uspto.gov]

Sent:

Monday, May 14, 2007 3:45 PM

To:

STIC-EIC1700

Subject:

Database Search Request, Serial Number: 10664818

Requester:

TONY CHUO (P/1745)

Art Unit:

GROUP ART UNIT 1745

Employee Number:

81950

Office Location:

REM 06C11

Phone Number:

(571)272-0717

Mailbox Number:

SCIENTIFIC REFERENCE BR Sci & rech Inf Cnt

MAY 1 5 RECD

Pat. & T.M Office

Case serial number:

10664818

Class / Subclass(es):

429/38

Earliest Priority Filing Date:

<u>9/16/03)</u>

Format preferred for results:

Paper

Search Topic Information:

A container that supplies a source of fuel to a direct methanol fuel cell, the container comprising:

a) a housing having at least a portion of the wall of the housing being comprised of a thermally conductive material, wherein the remaining portions of the walls of the container are thermally insulating;

b) a fuel egress port supported by the housing; and

c) a surface area planar vaporization membrane residing in the container.

Special Instructions and Other Comments:

=> fil wpix FILE 'WPIX' ENTERED AT 18:12:46 ON 24 MAY 2007 COPYRIGHT (C) 2007 THE THOMSON CORPORATION

FILE LAST UPDATED: 23 MAY 2007 <20070523/UP>
MOST RECENT THOMSON SCIENTIFIC UPDATE: 200733 <200733/DW>
DERWENT WORLD PATENTS INDEX SUBSCRIBER FILE, COVERS 1963 TO DATE

- >>> New reloaded DWPI Learn File (LWPI) available as well <<<
- >>> YOU ARE IN THE NEW AND ENHANCED DERWENT WORLD PATENTS INDEX <<<
- >>> New display format FRAGHITSTR available <<<
 SEE ONLINE NEWS and
 http://www.stn-international.de/archive/stn online news/fraghitstr ex.pdf</pre>
- >>> IPC Reform backfile reclassification has been loaded to 31 December 2006. No update date (UP) has been created for the reclassified documents, but they can be identified by 20060101/UPIC and 20061231/UPIC. <<</p>

FOR A COPY OF THE DERWENT WORLD PATENTS INDEX STN USER GUIDE, PLEASE VISIT:

http://www.stn-international.de/training_center/patents/stn_guide.pdf

FOR DETAILS OF THE PATENTS COVERED IN CURRENT UPDATES, SEE http://scientific.thomson.com/support/patents/coverage/latestupdates/

PLEASE BE AWARE OF THE NEW IPC REFORM IN 2006, SEE http://www.stn-international.de/stndatabases/details/ipc_reform.html and http://scientific.thomson.com/media/scpdf/ipcrdwpi.pdf

>>> FOR DETAILS ON THE NEW AND ENHANCED DERWENT WORLD PATENTS INDEX PLEASE SEE
http://www.stn-international.de/stndatabases/details/dwpi r.html <<<

=> d his nofile

(FILE 'HOME' ENTERED AT 17:06:53 ON 24 MAY 2007)

FILE 'HCAPLUS' ENTERED AT 17:07:00 ON 24 MAY 2007
L1 1 SEA ABB=ON PLU=ON US2005058879/PN

FILE 'REGISTRY' ENTERED AT 17:07:36 ON 24 MAY 2007
L2 2 SEA ABB=ON PLU=ON (1333-74-0/BI OR 67-56-1/BI)
D SCA

FILE 'HCAPLUS' ENTERED AT 17:17:28 ON 24 MAY 2007 QUE ABB=ON PLU=ON FUEL (A) CELL 17586 SEA ABB=ON PLU=ON (DELIVER? OF L3 L4 (DELIVER? OR SUPPLY? OR DIRECT?) (3A) (FUEL? OR METHANOL OR CH3OH) QUE ABB=ON PLU=ON DELIVER? OR SUPPLY? OR DIRECT? QUE ABB=ON PLU=ON FUEL? L5 L6 QUE ABB=ON PLU=ON METHANOL OR CH3OH OR MEOH
QUE ABB=ON PLU=ON ETHANOL OR PROPANOL OR ISOPROPANOL L7 L8 OR ETOH OR PROH OR IPROH OR (1 OR 2 OR I OR ISO) (W) (PROPA NOL OR PROH) L9 20530 SEA ABB=ON PLU=ON L5 (3A) (L6 OR L7 OR L8)

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L10
        8933 SEA ABB=ON PLU=ON L3 AND L9
L11
               QUE ABB=ON PLU=ON THERMAL? (2A) INSULAT? OR THERMOINSULAT
L12
            53 SEA ABB=ON PLU=ON L10 AND L11
               OUE ABB=ON PLU=ON THERMAL? (2A) CONDUCT? OR THERMOCONDUCT
L13
L14
          40 SEA ABB=ON PLU=ON L10 AND L13
            3 SEA ABB=ON PLU=ON L12 AND L14
L15
               OUE ABB=ON PLU=ON EVAPORAT? OR EVAPOURAT? OR VAPORIZ?
L16
               OR VAPOURIZ? OR VAPORIS? OR VAPOURIS?
L17
              QUE ABB=ON PLU=ON MEMBRANE
L18
            3 SEA ABB=ON PLU=ON (L12 OR L14) AND L16
            29 SEA ABB=ON PLU=ON (L12 OR L14) AND L17
L19
            2 SEA ABB=ON PLU=ON (L15 OR L18) AND L19
L20
            6 SEA ABB=ON PLU=ON L20 OR L15 OR L18
1.21
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         48088 SEA ABB=ON PLU=ON L5 (3A) (L6 OR L7 OR L8)
L23
         6980 SEA ABB=ON PLU=ON L23 AND L3
L24
           28 SEA ABB=ON PLU=ON L24 AND L11
L25
           36 SEA ABB=ON PLU=ON L24 AND L13
L26
            4 SEA ABB=ON PLU=ON L25 AND L26
L27
            9 SEA ABB=ON PLU=ON (L25 OR L26) AND L16
L28
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L29
            2 SEA ABB=ON PLU=ON L28 AND L29
L30
            5 SEA ABB=ON PLU=ON L27 OR L30
L31
    FILE 'COMPENDEX' ENTERED AT 17:51:40 ON 24 MAY 2007
T.32
           3 SEA ABB=ON PLU=ON L24 AND L11
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L33
            0 SEA ABB=ON PLU=ON L32 AND L33
L34
             1 SEA ABB=ON PLU=ON (L32 OR L33) AND L16
L35
            12 SEA ABB=ON PLU=ON (L32 OR L33) AND L17
L36
             O SEA ABB=ON PLU=ON L35 AND L36
L37
    FILE 'INSPEC' ENTERED AT 17:54:41 ON 24 MAY 2007
           2 SEA ABB=ON PLU=ON L24 AND L11
L38
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L39
            0 SEA ABB=ON PLU=ON L38 AND L39
0 SEA ABB=ON PLU=ON (L38 OR L39) AND L16
L40
L41
           16 SEA ABB=ON PLU=ON (L38 OR L39) AND L17
L42
             O SEA ABB=ON PLU=ON L42 AND L16(5A)L17
L43
    FILE 'PASCAL' ENTERED AT 18:05:45 ON 24 MAY 2007
        1 SEA ABB=ON PLU=ON L24 AND L11
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L45
            0 SEA ABB=ON PLU=ON L44 AND L45
L46
             O SEA ABB=ON PLU=ON (L44 OR L45) AND L16
L47
             6 SEA ABB=ON PLU=ON (L44 OR L45) AND L17
L48
             7 SEA ABB=ON PLU=ON L44 OR L48
L49
    FILE 'WPIX' ENTERED AT 18:10:51 ON 24 MAY 2007
              SEL L31 PN, APPS
    FILE 'HCAPLUS' ENTERED AT 18:11:04 ON 24 MAY 2007
     4 SEA ABB=ON PLU=ON (US2001-262991P/APPS OR US2001-263010
            5 SEA ABB=ON PLU=ON L21 NOT L50
L51
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FILE 'HCAPLUS, COMPENDEX, INSPEC, PASCAL' ENTERED AT 18:11:40 ON 24 MAY 2007

L52

14 DUP REM L51 L35 L38 L49 (1 DUPLICATE REMOVED)

=> d 131 ifull 1-5

L31 ANSWER 1 OF 5 WPIX COPYRIGHT 2007 THE THOMSON CORP on STN

ACCESSION NUMBER: 2006-564457 [58] WPIX

DOC. NO. NON-CPI: N2006-453644 [58]

TITLE: Heat exchange apparatus for electric vehicle, has foam material arranged at back side, so that sound

insulation property and thermal

conductivity was increased

DERWENT CLASS: X16; X21; X27

INVENTOR: TERASAKI T

PATENT ASSIGNEE: (NSMO-C) NISSAN MOTOR CO LTD

COUNTRY COUNT:

PATENT INFORMATION:

WEEK LA PG PATENT NO KIND DATE MAIN IPC ______

JP 2006205761 A 20060810 (200658)* JA 7[4]

APPLICATION DETAILS:

PATENT NO KIND APPLICATION DATE

JP 2006205761 A JP 2005-16757 20050125

PRIORITY APPLN. INFO: JP 2005-16757 20050125

INT. PATENT CLASSIF.:

IPC ORIGINAL: B60K0001-04 [I,A]; B60K0001-04 [I,C]; B60K0011-02

[I,C]; B60K0011-04 [I,A]; B60K0008-00 [I,A];

B60K0008-00 [I,C]

BASIC ABSTRACT:

JP 2006205761 A UPAB: 20060911

NOVELTY - The foam material (29) was arranged at the back side of the metal plate (27), so that the sound insulation property and thermal conductivity was

increased. The metal plate was arranged at the vehicle forward side into the air flow from the radiator (19) side. The heat exchanger (15) was arranged at the metal plate at the vehicle forward side of the outer wall section. The air flow path (3) directs the air to the fuel cell.

USE - For electric vehicle using fuel cell

ADVANTAGE - Reduces the noise generated, while preventing the reduction of the thermal radiation of the heat exchanger apparatus.

DESCRIPTION OF DRAWINGS - The figure shows the perspective diagram of the heat exchanger used for the air supply apparatus for fuel cells. (Drawing includes non-English language text).

Air flow path (3) Heat exchanger (15) Radiator (19) Metal plate (27) Foam material (29)

FILE SEGMENT:

MANUAL CODE: EPI: X16-C09; X16-K01; X21-A01F; X21-B01A; X27-F02C

L31 ANSWER 2 OF 5 WPIX COPYRIGHT 2007 THE THOMSON CORP on STN

ACCESSION NUMBER: 2006-211555 [22] WPIX

EPT

DOC. NO. CPI: C2006-069605 [22] DOC. NO. NON-CPI: N2006-182067 [22]

TITLE: Hydrogen storage apparatus comprises housing having internal volume and passageway from internal volume and through housing, the internal volume including

first material for absorbing hydrogen, and second

material

DERWENT CLASS: L03; Q31; X16

INVENTOR: GROSS K; GROSS K J

PATENT ASSIGNEE: (GROS-I) GROSS K; (GROS-I) GROSS K J

COUNTRY COUNT: 109

PATENT INFORMATION:

PATENT NO	KIND DATE	WEEK LA	A PG	MAIN IPC
US 20060051638	A1 20060309	(200622)* EN	7 27 [15]	

APPLICATION DETAILS:

PATENT NO	KIND		PLICATION	DATE
US 20060051638	A1		2004-934340	
WO 2006029027 7	Δ1	WO	2005-11531429	20050902

PRIORITY APPLN. INFO: US 2004-934340 20040903

INT. PATENT CLASSIF.:

IPC ORIGINAL: B65B0003-00 [I,A]; B65B0003-00 [I,C]; C01B0003-00

[I,A]; C01B0003-00 [I,C]; H01M0002-02 [I,A]; H01M0002-02 [I,C]; H01M0008-04 [I,A]; H01M0008-04 [I,A]; H01M0008-04 [I,C]; H01M0008-06 [I,A]; H01M0008-06 [I,A]; H01M0008-06 [I,C]; H01M0008-24

[I,A]; H01M0008-24 [I,C]

BASIC ABSTRACT:

US 20060051638 A1 UPAB: 20060331

NOVELTY - A hydrogen storage apparatus has housing having internal volume and passageway from the internal volume and through the housing. The internal volume includes a first material for absorbing hydrogen and a second material having a higher thermal conductivity than the first material.

DETAILED DESCRIPTION - An INDEPENDENT CLAIM is also included for an electric power system for a device comprising greater than or equal to2 electric power modules each electrically connected to one other of the electric power modules, where each of the electric power modules includes γ a fuel cell stack operable on hydrogen, and housing in contact with the fuel

cell and having internal volumes for storing hydrogen and an outlet to provide hydrogen released from the internal volume to the fuel cell, where the heat for releasing hydrogen is provided by the fuel cell and

wiring to provide power from the power modules.

USE - Used for storing hydrogen (claimed).

ADVANTAGE - The invention allows for improved heat transfer into and out of a hydrogen-storage material. The hydrogen-storage

material is segmented into internal volumes that allows for tailoring of the hydrogen storage capabilities and easy replacement of materials. The **fuel cell**-hydrogen storage system has improved thermal matching of the **fuel cell** and hydrogen-storage material.

DESCRIPTION OF DRAWINGS - The figure is a section showing an exploded view of hydride storage beds and **fuel** cells.

Fuel supply line (101)
Fuel cell (120a-d)
Nut (203)
Bipolar plates (223)
Seals (305)

TECHNOLOGY FOCUS:

MECHANICAL ENGINEERING - Preferred Materials: The first material includes greater than or equal to2 materials for absorbing hydrogen. The second material is consisting of a sintered metal, a metal foam or a metal wool. The internal volume includes hydrogen storage material comprising a hydride, a high surface area material, a hydrogen-containing compound, a metal and/or an alloy. The hydride is selected from the group consisting of an alanate, complex hydride, borohydride, ionic hydride, titanium hydride, aluminum hydride, magnesium hydride or intermetallic hydrides. The intermetallic hydride is a rare earth-nickel based hydride, zirconium-manganese based hydride or titanium-iron based hydride. The hydrogen-containing compound consists of amides and imides. It includes a silicon-based hydrogen compound or a carbon-based hydrogen compound.

Preferred Components: The internal volume further includes a spring. The housing further includes a porous material within the passageway. The internal volume includes interconnected cylindrical volumes. The apparatus comprises fuel cell (120a-d) stacks each operable on hydrogen and oxygen having 2 fuel stack sides; and housings each in contact with a substantial portion of a fuel cell stack side and having internal volume for storing hydrogen and passageway. It includes thermal insulation surrounding a portion of the fuel cell stack and the housing, and providing a gap for circulating a gas. It further includes a vacuum-tight container surrounding the fuel cell and the housing, and a gas source to provide a controllable pressure to the vacuum-tight container. It has a device to control heat loss from the fuel cell stack and the housing.

FILE SEGMENT:

CPI; GMPI; EPI

MANUAL CODE:

CPI: L03-E04

EPI: X16-C09; X16-F01

L31 ANSWER 3 OF 5 WPIX COPYRIGHT 2007

PIX COPYRIGHT 2007 THE THOMSON CORP on STN

ACCESSION NUMBER:

2005-282820 [29] WPIX

DOC. NO. NON-CPI:

N2005-231778 [29]

TITLE:

Container e.g. fuel cartridge, for

supplying source of fuel to

direct methanol fuel

cell system, has portion of housing wall

with thermally conductive

material, and fuel egress port that is supported by

housing

DERWENT CLASS:

Q13; X16

INVENTOR:

GUAY G G; GUAY G

PATENT ASSIGNEE:

(GILL-C) GILLETTE CO; (GUAY-I) GUAY G G

COUNTRY COUNT:

107

PATENT INFORMATION:

PAT	TENT NO	KINI	DATE	WEEK	LA	PG	MAIN IPC
WO EP BR	20050058879 2005034274 1668731 2004014414 1868086	A2 A2 A		(200677)	EN EN EN EN PT ZH	21[9]	·
JP.	2007506251	W	20070315	(200722)	ΔT	20	

APPLICATION DETAILS:

PATENT NO KIND	APPLICATION DATE
US 20050058879 A1	US 2003-664818 20030916
BR 2004014414 A	BR 2004-14414 20040908
CN 1868086 A	CN 2004-80029982 20040908
EP 1668731 A2	EP 2004-783382 20040908
WO 2005034274 A2	WO 2004-US29105 20040908
EP 1668731 A2	'WO 2004-US29105 20040908
BR 2004014414 A	WO 2004-US29105 20040908
JP 2007506251 W	WO 2004-US29105 20040908
JP 2007506251 W	JP 2006-526929 20040908

FILING DETAILS:

PATENT NO	KIND		PATENT NO	
EP 1668731	A2	Based on	 WO 2005034274 · A	
BR 2004014414	Α	Based on	WO 2005034274 A	
TP 2007506251	W	Rased on	WO 2005034274 A	

PRIORITY APPLN. INFO: US 2003-664818 20030916

INT. PATENT CLASSIF.:

MAIN: H01M002-14; H01M008-04

SECONDARY: B01B001-00; B01J004-04; B60K015-03

IPC ORIGINAL: H01M0008-04 [I,C]; H01M0008-04 [I,A]; H01M0008-04

[I,C]; H01M0008-10 [I,A]; H01M0008-10 [I,C]

IPC RECLASSIF.: B01B0001-00 [I,A]; B01B0001-00 [I,C]; B01J0004-00

[I,C]; B01J0004-04 [I,A]; B60K0015-03 [I,A]; B60K0015-03 [I,C]; H01M0002-14 [I,A]; H01M0002-14

[I,C]; H01M0008-04 [I,A]; H01M0008-04 [I,C]

BASIC ABSTRACT:

US 20050058879 A1 UPAB: 20051222

NOVELTY - The container e.g. fuel cartridge (12), has a housing whose portion has a **thermally conductive** material. A fuel egress port is supported by the housing. A surface area enhanced planar **vaporization membrane** (44) resides in the container. Remaining portions of the wall is **thermally insulated**. The container has a liquid source of hydrogen e.g. methanol. The **membrane** partitions a liquid phase to a vapor phase.

DETAILED DESCRIPTION - An INDEPENDENT CLAIM is also included for a method of using the container e.g. fuel cartridge.

USE - Used for supplying a source of fuel

to a direct methanol fuel

cell (DMFC) system.

ADVANTAGE - The portion of the housing wall has thermally conductive material that enhances a higher delivery rate of methanol in a vapor phase across the membrane to deliver vapor at the egress port of the container. The container allows the fuel cell to operate without a need for pumps or other active controls.

DESCRIPTION OF DRAWINGS - The drawing shows a block diagram depicting an electronic device that is powered by a fuel cell.

Portable electronic device (10)

Fuel cartridge (12) Interconnect (16) Fuel cell (18)

Vaporization membrane (44)

FILE SEGMENT:

GMPI; EPI

MANUAL CODE:

EPI: X16-C01C; X16-C15A; X16-C15C

L31 ANSWER 4 OF 5 WPIX COPYRIGHT 2007 THE THOMSON CORP on STN

ACCESSION NUMBER: 2005-100769 [11] WPIX

CROSS REFERENCE:

2004-118664

DOC. NO. CPI:

C2005-033695 [11]

DOC. NO. NON-CPI:

N2005-087538 [11]

TITLE:

Heating a subterranean formation for in situ mining of fluids e.g. oil and gas, involves inserting into a hole in the formation a heater comprising casing

and fuel cells, and operating the fuel cells to produce heat

and electricity

DERWENT CLASS:

H01; Q49; X16; X25

INVENTOR:

SAVAGE M T

PATENT ASSIGNEE:

(INDE-N) INDEPENDENT ENERGY PARTNERS INC; (SAVA-I)

SAVAGE M T

COUNTRY COUNT:

PATENT INFORMATION:

PATENT NO KIND DATE WEEK LA PG MAIN IPC ______

US 20050016729 A1 20050127 (200511) * EN 58[35]

CA 2484887 A1 20050415 (200532) EN B2 20070227 (200718) EN US 7182132

APPLICATION DETAILS:

PATENT NO KIND APPLICATION DATE

-----US 20050016729 A1 CIP of US 2002-53207 20020115 US 20050016729 A1 US 2003-687264 20031015

CA 2484887 A1

CA 2004-2484887 20041015

FILING DETAILS:

PATENT NO KIND PATENT NO

US 20050016729 A1 CIP of

PRIORITY APPLN. INFO: US 2003-687264 20031015 US 2002-53207 20020115

INT. PATENT CLASSIF.:

IPC ORIGINAL:
IPC RECLASSIF.:

E21B0036-00 [I,C]; E21B0036-04 [I,A] E21B0036-00 [I,A]; E21B0036-00 [I,C]; E21B0041-00 [I,A]; E21B0041-00 [I,C]; E21B0043-16 [I,C]; E21B0043-24 [I,A]; H01M0008-00 [N,A]; H01M0008-00 [N,C]; H01M0008-04 [I,A]; H01M0008-04 [I,C]; H01M0008-24 [I,A]; H01M0008-24 [I,C]

BASIC ABSTRACT:

US 20050016729 A1 UPAB: 20060121

NOVELTY - Heating a subterranean formation involves forming a hole into the formation; inserting into the hole a heater comprising a casing (34) and fuel cells (400) contained within the casing; operating the fuel cells so as to produce heat and electricity; and generating gaseous product, which is provided to and used by the fuel cells as fuel.

DETAILED DESCRIPTION - INDEPENDENT CLAIMS are also included for:

- (1) a subterranean formation heater comprising a casing (34) having fuel cells, where the fuel cells have a feedback connection to the subterranean formation for receiving a fuel from the formation, and where a total fuel used to power the fuel cells is supplied via the feedback connection; and
- (2) a conduction heater comprising fuel cells, conduit (299, 499) each being in gaseous communication with the fuel cells, and manifold comprising conduits but no fuel cells, where the manifold connects a planetary surface to the fuel cells;
- (3) a method to start up a down hole conduction heater comprising forming a stack (600) of **fuel cells** in a casing, inserting a stack down a borehole (300), feeding the stack with conduits to **supply** an oxidant and **fuel** to the stack, and bringing a temperature of the stack up to an operating temperature of 750-1000degreesC; and
- (4) a fuel cell assembly comprising an interconnect plate having a peripheral edge and having a heat conductive structure, fuel cells mounted adjacent to the peripheral edge, and channels to the fuel cell to provide fuel and oxidant and to transport exhaust gasses.

USE - The method is used for heating a subterranean formation for in situ mining of fluids including oil and gas.

ADVANTAGE - The method utilizes a fuel cell, which acts as both a heating element and a power generator, resulting in increased economic efficiency. It converts fuel to heat, like combustion heaters, avoiding the inefficiencies of electrical resistance heaters. It produces heat uniformly over the length of the heater, like electrical resistance heaters, while avoiding hot spots and uneven heating of combustion heaters. It also eliminates the problems associated with mixing fuel and air in flameless combustor heaters.

DESCRIPTION OF DRAWINGS - The figure is a cross-sectional view of Geothermic Fuel Cell Modules installed in a resource.

Casing (34) Conduit (299, 499) Borehole (300) Fuel cells (400) Fuel cell stack (600)

TECHNOLOGY FOCUS:

ELECTRICAL POWER AND ENERGY - Preferred Components: At least after an initial start-up period, the fuel cells are fueled by greater than or equal to10% of the gaseous product generated by the formation. Each fuel cell has a thickness and an active component surface. It generates a warm exhaust gas which is collected and used to heat the formation. The heater segment has greater than desired combined thermal output if the fuel cells were configured continuously within the segment. The stack of fuel cells is connected end to end to form a stick of fuel cell assemblies. An insulated current return cable is attached to a bottom of the string, thus forming a useful electric potential between a top of the string and the cable.

MECHANICAL ENGINEERING - Preferred Method: The method further comprises filling an annular gap, which is defined by the casing and the hole, with a **thermally conductive** substance. Preferred Components: The manifold comprises **thermal insulation** to inhibit transfer of heat from the manifold to a surrounding environment. It further comprises a heat exchanger. Spacer plates having aligned holes with the interconnect plates are provided to selectively reduce a heat output of the stick.

FILE SEGMENT: CPI; GMPI; EPI

MANUAL CODE: CPI: H01-D06B; H01-D08

EPI: X16-C15A; X16-C15A1; X16-C18; X25-E

L31 ANSWER 5 OF 5 WPIX COPYRIGHT 2007 THE THOMSON CORP on STN

ACCESSION NUMBER:

2003-029983 [02] WPIX

DOC. NO. CPI:

C2003-006866 [02]

DOC. NO. NON-CPI:

N2003-023711 [02]

TITLE:

Apparatus for electrochemical cell, has electrochemical cell electrically conductive support having conductive core which comprises active area covered with electrically and

thermally conductive polymeric

chermarry conductive porymer.

composite

DERWENT CLASS:

A85; E36; J03; L03; X16; X25

INVENTOR:

BAARS D M; BORGES H P; CHEN S B; EHRENBERG S G; EHRENBERT S G; FITTS B B; JOHNSON B C; LANDI V R;

ROY S K; CHUN S B

PATENT ASSIGNEE:

(BAAR-I) BAARS D M; (BORG-I) BORGES H P; (CHEN-I)
CHEN S B; (DAIS-N) DAIS-ANALYTIC CORP; (EHRE-I)
EHRENBERT S G; (FITT-I) FITTS B B; (JOHN-I) JOHNSON
B C; (LAND-I) LANDI V R; (ROYS-I) ROY S K; (WORL-N)

WORLD PROPERTIES INC

COUNTRY COUNT:

94

PATENT INFORMATION:

PAT	TENT NO	KINI	D DATE	WEEK	LA	PG	MAIN IPC
WO	2002080295	A2	20021010	(200302)*	EN	38[11]	
US	20020155333	A1	20021024	(200302)	EN		
GB	2389701	A	20031217	(200407)	EN		
US	20040076863	A1	20040422	(200428)	EN		
AU	2002312570	A1	20021015	(200432)	EN		
JP	2005502981	W	20050127	(200510)	JA	68	
DE	10295503	T 5	20050908	(200559)	DE		
US	7138203	B2	20061121	(200677)	EN		

APPLICATION DETAILS:

PATENT NO	KIND	AP	PLICATION DATE
WO 2002080295	A2	WO	2002-US19875 20020118
US 20020155333	A1 Provisional	US	2001-262991P 20010119
US 20020155333	Al Provisional	US	2001-263010P 20010119
US 20040076863	A1 Provisional '	US	2001-262991P 20010119
US 20040076863	Al Provisional	US	2001-263010P 20010119
AU 2002312570	A1	ΑU	2002-312570 20020118
DE 10295503 T5		DE	2002-10295503 20020118
JP 2005502981	W	JP	2002-578592 20020118
US 20020155333	A1	US	2002-53346 20020118
US 20040076863	A1 CIP of	US	2002-53346 20020118
GB 2389701 A		WO	2002-US19875 20020118
JP 2005502981	W	WO	2002-US19875 20020118
DE 10295503 T5		WO	2002-US19875 20020118
US 20040076863	A1	US	2003-638117 20030807.
GB 2389701 A		GB	2003-19464 20030819
US 7138203 B2	Provisional	US	2001-262991P 20010119
US 7138203 B2	Provisional	US	2001-263010P 20010119
US 7138203 B2	CIP of	US	2002-53346 20020118
US 7138203 B2		US	2003-638117 20030807

FILING DETAILS:

PATENT NO	KIND			PAT	ENT NO		
GB 2389701 A		Based	on	wo	2002080	295	 А
AU 2002312570 A	.1	Based	on	WO	2002080	295	Α
JP 2005502981 W	1	Based	on	WO	2002080	295	Α
DE 10295503 T5		Based	on	WO	2002080	295	Α

PRIORITY APPLN. INFO: US 2001-263010P 20010119

US 2001-262991P 20010119 US 2002-53346 20020118 US 2003-638117 20030807

INT. PATENT CLASSIF.:

MAIN: H01M008-02 SECONDARY: H01M008-24

IPC ORIGINAL: H01M0002-08 [I,A]; H01M0002-08 [I,C]; H01M0002-14

[I,A]; H01M0002-14 [I,C]; H01M0008-04 [I,A];

H01M0008-04 [I,C]

IPC RECLASSIF.: C25B0009-04 [I,A]; C25B0009-04 [I,C]; H01M0008-02

[I,A]; H01M0008-02 [I,C]; H01M0008-04 [N,A];

H01M0008-04 [N,C]

BASIC ABSTRACT:

WO 2002080295 A2 UPAB: 20060118

NOVELTY - An electrochemical cell apparatus has an electrochemical cell electrically conductive support (10) comprising a conductive core. The conductive core comprises an active area which is covered with an electrically and thermally conductive polymeric composite (12).

DETAILED DESCRIPTION - INDEPENDENT CLAIMS are included for the following:

(1) A system, which has conductive support, a gas supply unit for supplying fuel gases and oxidant gases to the fuel cell membranes, electrical unit for transporting electrical charge to and from the fuel cell membranes, electrical unit for conditioning power produced by fuel cell membranes, and control unit for controlling the fuel gases, oxidant gases and electrical unit; and

(2) An electrochemical cell component which has a conductive core, and an electrically and thermally conductive polymer composite covering and adhered to core by an adhesion promoter. The electrochemical cell component has a volume resistivity of 0.116 OMEGA cm or less.

USE - For electrochemical cell.

ADVANTAGE - The conductive support has excellent chemical resistance, resistance to hydrolysis, good mechanical integrity, roughness and good conductivity. The conductive support has a volume resistivity of 0.5 OMEGA cm or less, preferably 0.045 OMEGA cm or less and thermal conductivity of at least 5 watts/m K, preferably at least 13 watts/m K. The conductive support is produced economically from inexpensive raw materials. The connectors support allows the heat generated by the electrochemical cell to be laterally conducted and transferred to circulating fluids such as air, thus the complexity of the support and its manufacture are reduced. The use of thin layer of adhesion promoter between the core and the polymeric composite reduces the tendency of the core and polymeric composite to debond and disparity in the dimensional stability of the core and polymer composite, without decreasing electrical and thermal conductivity.

DESCRIPTION OF DRAWINGS - The figure shows the cross-sectional view of an electrochemical cell electrically conductive support.

Electrochemical cell electrically conductive support (10) Electrically and thermally conductive polymeric composite (12)

TECHNOLOGY FOCUS:

INORGANIC CHEMISTRY - Preferred Metal: The conductive core comprises a metal or metal alloy selected from aluminum, copper, nickel, platinum, titanium, gold plated metals, stainless steel and magnesium.

POLYMERS - Preferred Compounds: The conductive polymer composite is a polybutadiene- or polyisoprene-based composite which comprises conductive filler (10-90 volume%), thermosetting polybutadiene or polyisoprene resin, unsaturated butadiene- or isoprene-containing polymer, functionalized liquid polybutadiene or polyisoprene resin, and monomer(s) with vinyl unsaturation selected from styrene, vinyl toluene, divinyl benzene, triallylcyanurate, diallylphthalate, and multifunctional acrylate monomers. The conductor filler in the form of fiber and/or platelets, is synthetic graphite. The poly butadiene or polyisoprene resin is epoxidized phenol novalac resin or epoxidized cresol novalac resin. The unsaturated butadiene or isoprene-containing polymer is a copolymer of isoprene or butadiene and another monomer, or block copolymer such as styrene-butadiene or methyl styrene-butadiene di-block polymer or a thermoplastic elasotmer block copolymer. The adhesion promoter is silane such as mercapto-functional silane or vinyl silane, titanate, or zirconate adhesion promoter.

MECHANICAL ENGINEERING - Preferred Components: The conductive support further has at least one channel for conducting fluid which is an exterior channel for conducting fuel gas, fuel liquid, oxidant gas or oxidant liquid, or an interior channel for conducting cooling fluid. The conductive core further has heat

transfer area in a form of a cooling fin. Preferred Properties: A thermal coefficient of expansion of the conductive core is same as a thermal coefficient of expansion of the conductive polymer composite, over an operative temperature range of fuel cell. The conductive support has volume resistivity of less than 0.5 OMEGA cm and a thermal conductivity of at least 5 watts/meter degreesK.

EXTENSION ABSTRACT:

EXAMPLE - Aluminum plates with thickness of 0.07 cm, width of 10.7 cm and length of 11 cm, were lightly abraded with sand-paper or using other abrading units. The aluminum plates were then washed with acetone and then pretreated with A1106 (solution of amino silane) (5 weight% (weight%)), in acetone by dip coating. Then, the solvent was allowed to evaporate under ambient conditions. The plate was subsequently transferred to a preheated die. A conductive epoxy-based composite material comprising (in volume%) Sumiepoxy ESCN 195XL 25 (epoxidized cresol novolac resin) (11.73), Epiclon N-770 (epoxidized phenol novolac resin) (10.14), Asbury 3621 (natural graphite) (40.02), Asbury A99 (synthetic graphite) (20.69), calcium stearate (3.45), HRJ 11040 (phenol-formaldehyde polymer) (13.59), Ancamine K54 (2,4,6-tris dimethyl-amino methyl phenol) (0.21) and Lonzest GMS (glycerol mono stearate) (0.17), was filled in the mold cavity. The composite was compression molded onto the surface of the plate at 180degreesC mold temperature, 10000-12000 pounds/square inch (psi) cavity pressure for 4 minutes. The molded conductive polymer composite was cured at 240degreesC for 4 hours and an electrochemical cell electrically conductive support was obtained. An apparatus having the obtained support having active area covered with the polymeric composite, was obtained. The obtained support had very good electrical and solvent resistance properties and excellent mechanical integrity. The obtained support was rigid with good dimensional stability. As the obtained support was heated and cooled in cooling cycles, no bowing of the support was noted, thus temperature coefficient of expansion of the polymeric composite was same as the temperature coefficient of the aluminum. The obtained support had volume resistivity of 0.068 OMEGA-cm according to IPC TM-650 and a thermal conductivity of 13.4 watts/m K according to ASTM C518.

FILE SEGMENT: CPI; EPI

MANUAL CODE:

CPI: A04-B01E; A08-M09A; A08-R01; A09-A03; A12-E06;

E05-E01; E05-E02D; E05-G09A; E05-G09B; E05-L01;

E05-M; E35-L; J03-B02; L03-E04; L03-E04B

EPI: X16-C01; X16-E06A; X25-R01A

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FILE COVERS 1970 TO DATE.

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THE BASIC INDEX >>>

=> fil inspec

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FILE LAST UPDATED: 21 MAY 2007 <20070521/UP>
FILE COVERS 1898 TO DATE.

<<< SIMULTANEOUS LEFT AND RIGHT TRUNCATION AVAILABLE IN
THE ABSTRACT. (/AB), BASIC INDEX (/BI) AND TITLE (/TI) FIELDS >>>

=> fil pascal

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FILE LAST UPDATED: 21 MAY 2007 <20070521/UP>
FILE COVERS 1977 TO DATE.

>>> SIMULTANEOUS LEFT AND RIGHT TRUNCATION IS AVAILABLE IN THE BASIC INDEX (/BI) FIELD <><

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L52 ANSWER 1 OF 14 HCAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2006:1119155 HCAPLUS

DOCUMENT NUMBER: 145:457645

ENTRY DATE: Entered STN: 26 Oct 2006

TITLE: Novel materials for alkaline fuel

cells

INVENTOR(S): Abson, Nicholas M.; Middleton, Peter Hugh

PATENT ASSIGNEE(S): Fr.

SOURCE:

Eur. Pat. Appl., 8pp.

CODEN: EPXXDW

DOCUMENT TYPE:

Patent

LANGUAGE:

English

CLASSIFICATION:

52-2 (Electrochemical, Radiational, and Thermal

Energy Technology)

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO. KIND DATE APPLICATION NO. DATE

EP 1715538

A1 20061025 EP 2005-8535

200504

9

R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT, IE, SI, LT, LV, FI, RO, MK, CY, AL, TR, BG, CZ, EE, HU, PL, SK, BA, HR, IS, YU

PRIORITY APPLN. INFO.:

EP 2005-8535

200504

19

PATENT CLASSIFICATION CODES:

PATENT NO. CLASS PATENT FAMILY CLASSIFICATION CODES

[I,A]

ECLA H01M004/88; H01M008/02C4C; H01M008/08A

ABSTRACT:

This invention describes the use of conducting porous graphite foam materials as electrodes, catalyst supports, gas diffusion layers and other components in alkaline **fuel cells** and others such as the proton exchange **membrane fuel cell**.

The porous open structure of the graphite material is ideally suited to vapor deposition of catalyst materials. Porous graphite foams can be made by the pyrolysis of pitch at high temps. Alternatively they can be made by the pyrolysis of certain polymer compds. which can create a foam structure during the curing process. Although the exact microstructure of the final graphite foam depends on many factors, they all possess key phys. properties which are relevant to the invention described here such as high **thermal conductivity** and high elec. conductivity The foam can also be used in its powdered form as a conductive additive to gas diffusion layers, electrodes and bi-polar plates.

SUPPL. TERM:

fuel cell conducting porous

graphite foam material

INDEX TERM:

Fuel cells

(alkaline fuel cells; materials for

alkaline fuel cells)

INDEX TERM: ·

Fuel cell electrodes

(catalytic; materials for alkaline fuel

cells)

INDEX TERM:

Vapor deposition process

(chemical; materials for alkaline fuel

cells)

INDEX TERM:

Coating process

(dip; materials for alkaline fuel

cells)

INDEX TERM:

Fuel cells

(direct methanol; materials for

```
alkaline fuel cells)
INDEX TERM:
                   Catalysts
                       (electrocatalysts; materials for alkaline fuel
                       cells)
                   Coating process
INDEX TERM:
                       (electroless; materials for alkaline fuel
                       cells)
                   Spraying
INDEX TERM:
                       (electrospraying; materials for alkaline fuel
                       cells)
INDEX TERM:
                   Carbon fibers, uses
                   ROLE: DEV (Device component use); USES (Uses)
                       (fabrics, graphitized; materials for alkaline
                       fuel cells)
INDEX TERM:
                   Fuel cell electrodes
                       (gas diffusion; materials for alkaline fuel
                      cells)
INDEX TERM:
                   Electrodeposition
                     Evaporation
                   Screen printing
                   Sputtering
                       (materials for alkaline fuel cells)
INDEX TERM:
                   Borides
                   ROLE: CAT (Catalyst use); USES (Uses)
                       (materials for alkaline fuel cells)
INDEX TERM:
                   Fluoropolymers, processes
                   ROLE: PEP (Physical, engineering or chemical process);
                   PYP (Physical process); PROC (Process)
                       (materials for alkaline fuel cells)
INDEX TERM:
                   Perovskite-type crystals
                       (oxides; materials for alkaline fuel
                      cells)
INDEX TERM:
                   Foams
                       (porous graphite; materials for alkaline fuel
                      cells)
INDEX TERM:
                   Fuel cells
                       (proton exchange membrane; materials for
                      alkaline fuel cells)
INDEX TERM:
                   Vapor deposition process
                       (vacuum; materials for alkaline fuel
                      cells)
INDEX TERM:
                   Spraying
                       (wet; materials for alkaline fuel
                      cells)
INDEX TERM:
                   7440-02-0, Nickel, uses
                   ROLE: CAT (Catalyst use); USES (Uses)
                       (Raney; materials for alkaline fuel
                      cells)
INDEX TERM:
                   7782-42-5, Graphite, uses
                   ROLE: DEV (Device component use); USES (Uses)
                       (foam, porous; materials for alkaline fuel
                      cells)
INDEX TERM:
                   7440-06-4, Platinum, uses
                   ROLE: CAT (Catalyst use); USES (Uses)
                       (materials for alkaline fuel cells)
INDEX TERM:
                   9002-84-0, PTFE
                   ROLE: PEP (Physical, engineering or chemical process);
                   PYP (Physical process); PROC (Process)
                       (materials for alkaline fuel cells)
INDEX TERM:
                   67-56-1, Methanol, uses
```

ROLE: TEM (Technical or engineered material use); USES

(Uses)

5

(materials for alkaline fuel cells)

INDEX TERM:

7440-44-0, Carbon, uses

ROLE: DEV (Device component use); USES (Uses) (paper, graphitized; materials for alkaline

fuel cells)

REFERENCE COUNT:

THERE ARE 5 CITED REFERENCES AVAILABLE FOR THIS RECORD.

REFERENCE(S):

- (1) Cisar; US 6054228 A 2000 HCAPLUS
- (2) Dornier Gmbh; DE 19647534 A1 1998 HCAPLUS
- (3) Licentia Patent-Verwaltungs-Gmbh; DE 2101777 A1 1972 HCAPLUS
- (4) Licentia Patentverwaltungs Gmbh; GB 1379846 A 1975
- (5) Mitsubishi Gas Chemical Company Inc; EP 1225160 A 2002 HCAPLUS

L52 ANSWER 2 OF 14 PASCAL COPYRIGHT 2007 INIST-CNRS. ALL RIGHTS RESERVED. on STN

ACCESSION NUMBER:

2006-0273691 PASCAL

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CORPORATE SOURCE:

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reserved.

TITLE (IN ENGLISH):

Proton conductivity and characterization of

novel composite membranes for medium-temperature fuel cells International Congress on Membranes and Membrane Processes: August 21-26,

2005, Seoul, Korea

AUTHOR:

AHMAD M. I.; ZAIDI S. M. J.; RAHMAN S. U. Department of Chemical Engineering, King Fahd

University of Petroleum & Minerals (KFUPM),

Dhahran-31261, Saudi Arabia

SOURCE:

Desalination : (Amsterdam), (2006), 193(1-3),

387-397, 17 refs.

Conference: ICOM International Congress on Membranes and Membrane Processes, Seoul (Korea,

Republic of), 21 Aug 2005 ISSN: 0011-9164 CODEN: DSLNAH

DOCUMENT TYPE:

Journal; Conference

BIBLIOGRAPHIC LEVEL: COUNTRY:

Analytic Netherlands English

LANGUAGE:

ABSTRACT:

INIST-12906, 354000142613670520

AVAILABILITY:

Direct methanol fuel

cells (DMFC) have received considerable

attention both as a portable power source and as

a replacement for batteries. The available

conventional Nafion membranes currently used in hydrogen fuel

cells are not suitable for use in DMFC due to their dehydration and instability at temperatures higher than 100°C. Novel

composite membranes have been prepared with the help of a sulfonated polyether ether

ketone (SPEEK) polymer and a novel solid proton conductor, namely heteropolyacid-loaded

Y-zeolite. The novel solid proton conductor has

high proton conductivity and high thermal and structural stability because

of the presence of Y-zeolite. The conductivity

of the composite membranes at room

temperature as well as at higher temperatures was found to increase with the incorporation of solid conducting material particles into the SPEEK polymer. The conductivity increased by 3-4 times at room temperature and increased to

times at room temperature and increased to exceptionally high values at temperatures higher

than 100°C. In all cases the presence of

the solid proton conductor led to an increase in

conductivity of the membranes without

detriment to their flexibility. Water uptake of

the membranes also followed a similar trend as that of conductivity. The membranes were characterized by XRD,

FTIR and SEM techniques, which confirmed even distribution of solid material into the SPEEK polymer. Hence, these low-cost membranes

can be considered for use in DMFC for portable

devices as well as for medium-temperature

stationary applications.

CLASSIFICATION CODE:

001D16; Applied sciences; Pollution, Nuisances 001D06D03E; Applied sciences; Energy; Thermal

use of fuels 230; Energy

CONTROLLED TERM:

Composite material; Fuel cell

; Hydrogen fuel cells;

Dehydration; Instability; Conducting material;

Zeolite; Stability; Flexibility; Water

absorption; Trend analysis; Scanning electron

microscopy

L52 ANSWER 3 OF 14 HCAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2005:1191997 HCAPLUS 143:462855

ENTRY DATE:

Entered STN: 09 Nov 2005

TITLE:

Electrically heated reactor for gas phase

reforming to produce syngas

INVENTOR (S):

Laflamme, Claude B.; Petitclerc, Michel;

Labrecque, Raynald

PATENT ASSIGNEE(S):

Hydro-Quebec, Can.

SOURCE:

Can. Pat. Appl., 99 pp.

CODEN: CPXXEB

DOCUMENT TYPE:

Patent

LANGUAGE:

English

INT. PATENT CLASSIF.:

MAIN:

C01B003-32

SECONDARY: CLASSIFICATION:

C10L003-00; C01B003-02; B01J019-08; C01B003-36 51-11 (Fossil Fuels, Derivatives, and Related

Products)

Section cross-reference(s): 47

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
CA 2469859	A1	20051105	CA 2004-2469859	

200405

05

PRIORITY APPLN. INFO.:

CA 2004-2469859

200405 05

PATENT CLASSIFICATION CODES:

PATENT NO.	CLASS	PATENT FAMILY CLASSIFICATION CODES
CA 2469859	ICM	C01B003-32
	ICS	C10L003-00; C01B003-02; B01J019-08; C01B003-36
	IPCI	C01B0003-32 [ICM,7]; C10L0003-00 [ICS,7];
		C01B0003-02 [ICS,7]; B01J0019-08 [ICS,7];
		C01B0003-36 [ICS,7]; C01B0003-00 [ICS,7,C*]
	IPCR	B01J0019-08 [I,C*]; B01J0019-08 [I,A];
		C01B0003-00 [I,C*]; C01B0003-02 [I,A];
		C01B0003-32 [I,A]; C01B0003-34 [I,A]; C01B0003-36
		[I,A]; C01B0003-38 [I,A]; C10L0003-00 [I,C*];
		C10L0003-00 [I,A]
	ECLA	B01D053/32B; B01J008/02B4; B01J008/02H;
		B01J019/08D2; B01J019/24R6; C01B003/34G;
		C01B003/38D

ABSTRACT:

SUPPL. TERM:

A reactor for reforming a hydrocarbon-containing gas in the presence of an oxidant to produce syngas consists of a housing, and a reaction chamber equipped with two electrodes and filled with a thermally

conductive , catalytically active material. The filling is elec.
insulated from the metal walls of the reactor housing. The electrodes are hollow and consist of a tube and a perforated disk being in contact with the reactor filling. One of the electrodes is the conduit for feeding the gas being reformed and the oxidant. The other electrode serves as an outlet of the reformate. The reactor filling is soft steel wool containing at least 80% group VIII elements, preferably Fe, Ni, and Co. The hydrocarbon feed can be natural gas, biogas, and C1-12 hydrocarbons. The oxidant can be CO2, CO, H2O, O2, or NOx. The hydrocarbon feed can contain sulfur which reacts with the reactor filling. The produced synthesis gas can be used for the production of methanol, and hydrogen supply of fuel cells.

elec heated reactor electrode hydrocarbon gas

		reforming oxidant syngas
INDEX	TERM:	Fuel gases
		(biogas; elec. heated reactor for gas phase
		reforming to produce syngas)
INDEX	TERM:	Electric heating
		Electrolytic cells
		Steam
		Synthesis gas
		(elec. heated reactor for gas phase reforming to
	•	produce syngas)
INDEX	TERM:	Fluoropolymers, uses
		ROLE: CAT (Catalyst use); DEV (Device component use);
		USES (Uses)
		(elec. heated reactor for gas phase reforming to
		produce syngas)
TNDEX	TERM:	Natural gas, reactions
		ROLE: CPS (Chemical process); PEP (Physical,
		engineering or chemical process); RCT (Reactant); PROC
		(Process); RACT (Reactant or reagent)
		(elec. heated reactor for gas phase reforming to
		produce syngas)
INDEX	TERM:	Electrodes
		(hollow; elec. heated reactor for gas phase
		(modelou, order, mondous reactor for Jub phase

reforming to produce syngas) INDEX TERM: Synthesis gas manufacturing (reforming synthesis gas manufacturing; elec. heated reactor for gas phase reforming to produce syngas) INDEX TERM: Asbestos ROLE: CAT (Catalyst use); DEV (Device component use); USES (Uses) (thermal insulator; elec. heated reactor for gas phase reforming to produce syngas) INDEX TERM: 9002-84-0, Teflon ROLE: CAT (Catalyst use); DEV (Device component use); USES (Uses) (Teflon, elec. insulator; elec. heated reactor for gas phase reforming to produce syngas) INDEX TERM: 630-08-0P, Carbon monoxide, preparation 1333-74-0P, Hydrogen, preparation ROLE: CPS (Chemical process); IMF (Industrial manufacture); PEP (Physical, engineering or chemical process); PREP (Preparation); PROC (Process) (elec. heated reactor for gas phase reforming to produce syngas) INDEX TERM: 74-82-8, Methane, reactions 124-38-9, Carbon dioxide, reactions ROLE: CPS (Chemical process); PEP (Physical, engineering or chemical process); RCT (Reactant); PROC (Process); RACT (Reactant or reagent) (elec. heated reactor for gas phase reforming to produce syngas) INDEX TERM: 11121-90-7, Carbon steel, uses ROLE: CAT (Catalyst use); DEV (Device component use); USES (Uses) (electrodes; elec. heated reactor for gas phase reforming to produce syngas) 1344-28-1, Alumina, uses INDEX TERM: ROLE: CAT (Catalyst use); DEV (Device component use); USES (Uses) (interior reactor wall coating; elec. heated reactor for gas phase reforming to produce syngas) INDEX TERM: 869003-17-8, BullDog, uses ROLE: CAT (Catalyst use); DEV (Device component use); USES (Uses) (reactor filling; elec. heated reactor for gas phase reforming to produce syngas) INDEX TERM: 12597-68-1, Stainless steel, uses ROLE: DEV (Device component use); USES (Uses) (reactor wall; elec. heated reactor for gas phase reforming to produce syngas) L52 ANSWER 4 OF 14 HCAPLUS COPYRIGHT 2007 ACS on STN ACCESSION NUMBER: 2004:820248 HCAPLUS DOCUMENT NUMBER: 141:317224 ENTRY DATE: Entered STN: 07 Oct 2004 TITLE: Fuel cell power generator for mobile electronic appliance INVENTOR(S): Yamauchi, Hisashi; Matsuoka, Takashi; Takashita, Masahiro; Akita, Masato PATENT ASSIGNEE(S): Toshiba Corp., Japan

Jpn. Kokai Tokkyo Koho, 23 pp.

CODEN: JKXXAF

SOURCE:

DOCUMENT TYPE:

Patent Japanese

LANGUAGE:

INT. PATENT CLASSIF.:

MAIN:

H01M008-24

SECONDARY:

H01M008-04; H01M008-10

CLASSIFICATION:

52-2 (Electrochemical, Radiational, and Thermal

Energy Technology)

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
				•
				•
JP 2004281072	Α	20041007	JP 2003-66766	
				200303
				12
PRIORITY APPLN. INFO.:			JP 2003-66766	
				200303
			•	10

PATENT CLASSIFICATION CODES:

PATENT NO.	CLASS	PATENT FAMILY CLASSIFICATION CODES
JP 2004281072	ICM	H01M008-24
UP 2004281072	ICS	H01M008-24 H01M008-04; H01M008-10
	IPCI	H01M0008-24 [ICM,7]; H01M0008-04 [ICS,7];
		H01M0008-10 [ICS,7]
	IPCR	H01M0008-04 [I,A]; H01M0008-04 [I,C*];
		H01M0008-10 [N,A]; H01M0008-10 [N,C*];
		H01M0008-24 [I,A]; H01M0008-24 [I,C*]
•	FTERM	5H026/AA08; 5H026/CX05; 5H026/HH00; 5H026/HH02;
		5H026/HH06; 5H027/AA08; 5H027/BA13

ABSTRACT:

The claimed power plant is equipped with a plurality of stacks consisting of laminated unit cells, where the each stack is covered with a heat ***insulating*** layer showing thermal conductivity \leq 0.1 (W/m/K) and satisfies P/S 20-31 (P = power output (mW) of the each stack; S = surface area (cm2) of the each stack). The power generator, especially suitable for direct-methanol ***fuel*** cells, provides high volume efficiency and power output.

SUPPL. TERM:

INDEX TERM:

direct methanol fuel cell heat insulator Thermal insulators

(fuel cell power generator

containing heat insulator for mobile electronic

appliance)

INDEX TERM:

Fuel cells

(power plants; fuel cell power

generator containing heat insulator for mobile

electronic appliance)

L52 ANSWER 5 OF 14 HCAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2004:77098 HCAPLUS

DOCUMENT NUMBER:

140:131103

ENTRY DATE:

Entered STN: 30 Jan 2004

TITLE:

Fuel cell having heat

conduction mechanism and small electric devices

INVENTOR(S):

Nakakubo, Toru; Eguchi, Takeshi; Watabe,

Mitsuhiro

PATENT ASSIGNEE(S):

Canon Inc., Japan

SOURCE:

Jpn. Kokai Tokkyo Koho, 22 pp.

CODEN: JKXXAF

DOCUMENT TYPE:

Patent

LANGUAGE:

Japanese

INT. PATENT CLASSIF.:

MAIN:

H01M008-04 H01M008-10

SECONDARY: CLASSIFICATION:

52-2 (Electrochemical, Radiational, and Thermal

Energy Technology)

Section cross-reference(s): 76

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
JP 2004031096	Α	20040129	JP 2002-185052	

25

PRIORITY APPLN. INFO.:

JP 2002-185052

200206

200206

PATENT CLASSIFICATION CODES:

PATENT NO.	CLASS	PATENT FAMILY CLASSIFICATION CODES .
JP 2004031096	ICM	H01M008-04
	TCC	1101M000 10

H01M008-10 ICS

H01M0008-04 [ICM, 7]; H01M0008-10 [ICS, 7] IPCI H01M0008-10 [I,C*]; H01M0008-10 [I,A]; IPCR H01M0008-04 [I,C*]; H01M0008-04 [I,A]

5H026/AA06; 5H026/CC01; 5H026/CX04; 5H026/HH03; FTERM 5H026/HH06; 5H026/HH08; 5H027/AA06; 5H027/CC02; 5H027/CC03; 5H027/CC04; 5H027/CC06; 5H027/CC15; 5H027/DD00; 5H027/KK46; 5H027/KK48

ABSTRACT:

The fuel cell comprises a fuel tank, an elec.

generator cell, a cylinder covering the elec. generator cell, wherein the fuel tank has a heat insulating structure therein, or a heat conduction mechanism having smaller heat resistance than that of the natural heat conduction is disposed between the elec. generator cell and the cylinder. The heat conduction mechanism maintains temps. in the fuel at an appropriate temperature for the high output voltage. ***cell***

SUPPL. TERM:

fuel cell heat conduction

mechanism small elec device; direct

methanol fuel cell DMFC;

polymer electrolyte fuel cell PEFC

INDEX TERM:

Electric apparatus

Fuel cells

Thermal conductors Thermal insulators (fuel cell having heat

conduction mechanism for small elec. devices)

L52 ANSWER 6 OF 14 COMPENDEX COPYRIGHT 2007 EEI on STN

ACCESSION NUMBER:

2004 (36):4394 COMPENDEX

TITLE:

SOFC anode recycle effect on diesel reforming.

AUTHOR: Borup, Rodney L. (Los Alamos National Lab.

MST-11 MS J579, Los Alamos, NM 87545, United States); Inbody, Michael A.; Tafoya, Jose I.;

Guidry, Dennis R.; Parkinson, W. Jerry

MEETING TITLE: 2004 AICHE Spring National Meeting, Conference

Proceedings.

MEETING ORGANIZER: American Institute of Chemical Engineers, AIChE

MEETING LOCATION: New Orleans, LA, United States

MEETING DATE: 25 Apr 2004-29 Apr 2004

SOURCE: 2004 AIChE Spring National Meeting, Conference

Proceedings 2004.p 147-154

SOURCE: 2004 AICHE Spring National Meeting, Conference

Proceedings 2004.p 147-154

ISBN: 0816909423

PUBLICATION YEAR: 2004 MEETING NUMBER: 63429

DOCUMENT TYPE: Conference Article

TREATMENT CODE: Theoretical; Experimental

LANGUAGE: English

ABSTRACT: Diesel fuel reforming was conducted

under iso-thermal conditions and under

real adiabatic conditions examining reforming

operating conditions such as solid oxide

fuel cells (SOFC) anode

recycle and carbon formation. Direct fuel injection via a fuel nozzle for

adiabatic operation was developed. The control of the fuel/air feed temperature was critical to

prevent pre-vaporization and vapor

locking of the fuel nozzle. Short periods of operation show stable performance, but catalyst deactivation was observed upon shut-down and restart of the reformer. (Edited abstract)

CLASSIFICATION CODE: 702.2 Fuel Cells; 802.2 Chemical Reactions; 714.1 Electron Tubes; 452.3 Industrial Wastes;

803 Chemical Agents; 804 Chemical Products

Generally

CONTROLLED TERM: *Solid oxide fuel cells;

Computer simulation; Nozzles; Diesel fuels; Heat exchangers; Integration; Reforming reactions;

Anodes; Recycling; Catalysts

SUPPLEMENTARY TERM: Infrastructures; Diesel reforming; Vehicular

auxiliary power units; Anode exhausts

L52 ANSWER 7 OF 14 PASCAL COPYRIGHT 2007 INIST-CNRS. ALL RIGHTS

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ACCESSION NUMBER: 2004-0213093 PASCAL

TITLE (IN ENGLISH): Direct synthesis of sulfonated aromatic

poly(ether ether ketone) proton exchange

membranes for fuel cell applications

AUTHOR: GIL M.; JI X.; LI X.; NA H.; HAMPSEY J. E.; LU

Υ.

CORPORATE SOURCE: Department of Chemistry Jilin University,

Changchun 130021, China

SOURCE: Journal of Membrane Science, (2004), 234(1-2),

75-81, 15 refs.

ISSN: 0376-7388 CODEN: JMESDO

DOCUMENT TYPE: Journal BIBLIOGRAPHIC LEVEL: Analytic

COUNTRY: LANGUAGE: AVAILABILITY: ABSTRACT: Netherlands English INIST-17232

Proton exchange membrane fuel cells (PEMFC) are promising no

cells (PEMFC) are promising new power sources for vehicles and portable devices.

Membranes currently used in PEMFC are

perfluorinated polymers such as Nafionoregistered trademark

Even though such membranes have demonstrated good performances and long-term

stability, their high cost and methanol

crossover makes them unpractical for large-scale production. Sulfonated aromatic poly(ether ether

ketones) (S-PEEKs) based membranes

have been studied due to their good mechanical

properties, thermal stability and conductivity. In this study, PEEK membranes directly prepared from the

sulfonated monomer were evaluated for possible

fuel cell applications by

determining the degree of sulfonation, water swelling, proton conductivity, methanol diffusivity and thermal stability. As synthesized S-PEEK membranes exhibit conductivities (25°C) from 0.02 to

0.07S/cm, water swelling from 13 to 54%, ion-exchange capacities (IEC) from 0.7 to 1.5meq/g and methanol diffusion coefficients from 3 x 10-7 to 5 x 10 -8cm2/s at 25°C.

These diffusion coefficients are much lower than

that of Nafion registered

trademark<pilcrow> (2 x 10 -6cm 2/s), making

S-PEEK membranes a good alternative to reduce problems associated with high methanol crossover in direct

methanol fuel cells.

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reserved.

001D07; Applied sciences; Chemical engineering 001D09; Applied sciences; Physicochemistry of polymers, Macromolecular chemistry, Materials

science

001D08A03; Applied sciences; Chemistry; Chemical

industry

001D06D03E; Applied sciences; Energy; Thermal

use of fuels

001B30; Physics; Atomic physics, Molecular

physics

001B00C40; Physics; Classical physics

230; Energy

CONTROLLED TERM: Proton exchange membranes (PEM);

Proton exchange membrane fuel

cells (PEMFC); Proton conductivity;

Ion-exchange capacities; Application; Polyether

ether ketones; Aromatic compounds; Fuel cells; Protons; Methanol; Diffusion;

Thermodynamic stability; Synthesis (chemical);

Ion exchange membranes; Theory;

Experiments

MHuang REM4B31 571-272-3952

CLASSIFICATION CODE:

L52 ANSWER 8 OF 14 INSPEC (C) 2007 IET on STN ACCESSION NUMBER: 2004:8006116 INSPEC

DOCUMENT NUMBER:

B2004-08-8410G-015

TITLE:

A microreactor for hydrogen production in micro

fuel cell applications

AUTHOR:

SOURCE:

Pattekar, A.V.; Kothare, M.V. (Dept. of Chem.

Eng., Lehigh Univ., Bethlehem, PA, USA)

Journal of Microelectromechanical Systems (Feb.

2004), vol.13, no.1, p. 7-18, 31 refs.

CODEN: JMIYET, ISSN: 1057-7157

SICI: 1057-7157(200402)13:1L.7:MHPM;1-N

Price: 1057-7157/04/\$20.00 Published by: IEEE, USA

DOCUMENT TYPE: TREATMENT CODE:

Journal Experimental United States

COUNTRY:

English

ABSTRACT:

LANGUAGE:

A silicon-chip based microreactor has been successfully fabricated and tested for carrying out the reaction of methanol reforming for microscale hydrogen production. The developed microreactor in combination with a micro

fuel cell is proposed as an

alternative to conventional portable sources of electricity such as batteries due to its ability

to provide an uninterrupted supply of electricity as long as a supply of methanol and water can be provided. The

microreformer-fuel cell

combination has the advantage of not requiring

the tedious recharging cycles needed by

conventional rechargeable lithium-ion batteries. It also offers significantly higher energy storage densities, which translates into less frequent 'recharging' through the refilling of methanol fuel. The microreactor consists of a

network of catalyst-packed parallel

microchannels of depths ranging from 200 to 400 μm with a catalyst particle filter near the outlet fabricated using photolithography and deep-reactive ion etching (DRIE) on a silicon substrate. Issues related to microchannel and filter capping, on-chip heating and temperature sensing, introduction and trapping of catalyst

particles in the microchannels, flow

distribution, microfluidic interfacing, and

thermal insulation have been

addressed. Experimental runs have demonstrated a methanol to hydrogen molar conversion of at least 85% to 90% at flow rates enough to supply

hydrogen to an 8- to 10-W fuel

cell

CLASSIFICATION CODE: B8410G Fuel cells; B8210 Energy resources;

> B2575F Fabrication of micromechanical devices; B2575D Design and modelling of micromechanical

devices

CONTROLLED TERM:

catalysis; chemical reactors; hydrogen economy; microfluidics; micromachining; photolithography;

proton exchange membrane fuel

cells; sputter etching

SUPPLEMENTARY TERM: hydrogen production microreactor; micro fuel

cells; microfluidics; microreformer;

system-on-chip; silicon-chip based microreactor; microscale hydrogen production; catalyst-packed

parallel microchannels; photolithography; deep-reactive ion etching; filter capping; on-chip heating; temperature sensing; thermal

insulation; methanol to hydrogen molar conversion; proton exchange membrane fuel cells;

catalytic steam reforming; 8 to 10 W; H

CHEMICAL INDEXING: H el

PHYSICAL PROPERTIES: power 8.0E+00 to 1.0E+01 W

ELEMENT TERMS: W

L52 ANSWER 9 OF 14 HCAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2003:364208 HCAPLUS

DOCUMENT NUMBER: 139:135926

ENTRY DATE: Entered STN: 13 May 2003

TITLE: Monolithic integrated fuel processor for the

conversion of liquid methanol

AUTHOR(S): Schuessler, M.; Portscher, M.; Limbeck, U.

CORPORATE SOURCE: Ballard Power Systems AG, Kirchheim/Teck-Nabern,

73230, Germany

SOURCE: Catalysis Today (2003), 79-80, 511-520

CODEN: CATTEA; ISSN: 0920-5861

PUBLISHER: Elsevier Science B.V.

DOCUMENT TYPE: Journal LANGUAGE: English

CLASSIFICATION: 52-1 (Electrochemical, Radiational, and Thermal

Energy Technology)

ABSTRACT:

Using a liquid fuel to run a fuel cell system becomes more attractive, when a simple and robust fuel processor can be developed. Conversion of a liquid methanol/water-mixture needs process steps to supply hydrogen to a fuel cell. Based on an approach using new material these processes are combined in an integrated fuel processor (IFP). The authors apply technologies from powder metallurgy like pressing and sintering, to fix catalyst powder and to shape complex functional structures. As a consequence of the new material approach, the IFP can be built as a monolith without any sealing. The good isotropic heat conductivity helps to ***thermally*** couple the processes. Exptl. results on a level of .apprx.20 L of hydrogen per min demonstrate the feasibility of the

.apprx.20 L of hydrogen per min demonstrate the feasibility of the concept. Supported by modeling, alternative schemes of reactor design indicate potential for optimization.

SUPPL. TERM: monolithic integrated fuel steam reforming methanol

porous ceramic catalyst; multifunctional reactor

catalyst fixation carbon monoxide oxidn

INDEX TERM: Sintering

(at 500-700° to make porous materials;

monolithic integrated fuel processor for conversion

of liquid methanol by steam reforming)

INDEX TERM: Fuel cells

Mechanical alloying Steam reforming

Steam reforming catalysts

(monolithic integrated fuel processor for

conversion of liquid methanol by steam reforming)

INDEX TERM: Simulation and Modeling (of reformate composition from various gas-mixing designs; monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: Capillary tubes (porous, aid vaporization; monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: Ceramics (porous, catalysts and gas distributors; monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: Models (physical) (prototypes; monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: Oxidation (selective; monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: 7440-50-8, Copper, uses ROLE: CAT (Catalyst use); DEV (Device component use); PEP (Physical, engineering or chemical process); PYP (Physical process); PROC (Process); USES (Uses) (catalyst support matrix and device construction; monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: 124-38-9, Carbon dioxide, processes 630-08-0, Carbon monoxide, processes ROLE: CPS (Chemical process); FMU (Formation, unclassified); PEP (Physical, engineering or chemical process); FORM (Formation, nonpreparative); PROC (Process) (monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: 67-56-1, Methanol, uses 118240-86-1, Methanol/water-mixture ROLE: CPS (Chemical process); PEP (Physical, engineering or chemical process); TEM (Technical or engineered material use); PROC (Process); USES (Uses) (monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: 7429-90-5, Aluminum, uses ROLE: DEV (Device component use); USES (Uses) (monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: 1333-74-0P, Hydrogen, uses ROLE: IMF (Industrial manufacture); RCT (Reactant); TEM (Technical or engineered material use); PREP (Preparation); RACT (Reactant or reagent); USES (Uses) (monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: 7440-06-4, Platinum, uses ROLE: CAT (Catalyst use); USES (Uses) (oxidation catalyst, in alumina-based binder; monolithic integrated fuel processor for conversion of liquid methanol by steam reforming) INDEX TERM: 131064-29-4, Copper zinc oxide ROLE: CAT (Catalyst use); DEV (Device component use); USES (Uses) (reforming catalyst; monolithic integrated fuel processor for conversion of liquid methanol by steam

reforming)

INDEX TERM:

1344-28-1, Alumina, uses

ROLE: CAT (Catalyst use); USES (Uses)

(support for platinum; monolithic integrated fuel processor for conversion of liquid methanol by steam reforming)

REFERENCE COUNT:

THERE ARE 16 CITED REFERENCES AVAILABLE FOR THIS RECORD.

REFERENCE(S):

- (1) Anon; US 5534328 1996
- (2) Anon; DE 19853379 1998 HCAPLUS
- (3) Anon; DE 19944187 1999 HCAPLUS
- (4) Anon; DE 10039592 2000 HCAPLUS
- (5) Anon; DE 10046692 2000 HCAPLUS
- (6) Anon; DE 102142933 2002
- (7) Daimler, C; Publication: Necar 5-driving with methanol 2000
- (8) Ehrfeld, W; Microreactors: New Technology for Modern Chemistry 2000
- (9) Hessel, V; Chemie Ingenieur und Technik 2002, V74, P185 HCAPLUS
- (10) Jeschar, R; Grundlagen der Warmeubertragung 1990, V3
- (11) Kahlich, M; J Catal 1997, V171, P93 HCAPLUS
- (12) Reuse, P; Proceedings of the Fifth International Conference on Microreaction Technology 2001
- (13) Ruselowski, G; http://www.transportation.anl.gov/ ttrdc/publications/index.html 2001
- (14) Schussler, M; Chem Eng Technol 2001, V24(11), P1141
- (15) Schussler, M; Fortschritt-Berichte Reihe 6 1998,
 401
- (16) Willer, B; Ph D Thesis, Universitat GH Kassel 1984

L52 ANSWER 10 OF 14

ACCESSION NUMBER:

DOCUMENT NUMBER:

TITLE:

INSPEC (C) 2007 IET on STN DUPLICATE 1

2002:7279583 INSPEC

A2002-13-8630G-008; B2002-07-8255-002 Operating experience with a 250 kWel molten

carbonate fuel cell (MCFC)

power plant

AUTHOR:

Bischoff, M.; Huppmann, G. (Energy Technol., MTU

Friedrichshafen GmbH, Munchen, Germany)

SOURCE:

Journal of Power Sources (20 March 2002),

vol.105, no.2, p. 216-21

CODEN: JPSODZ, ISSN: 0378-7753

SICI: 0378-7753 (20020320) 105:2L.216:0EWK; 1-Z

Price: 0378-7753/02/\$22.00 Doc.No.: S0378-7753(01)00942-9 Published by: Elsevier, Switzerland

Conference: Seventh Ulmer Elektrochemische Tage (Ulm Electrochemical Days), Ulm, Germany, 26-27

June 2000

DOCUMENT TYPE:

Conference; Conference Article; Journal

TREATMENT CODE: Practical COUNTRY: Switzerland LANGUAGE: English

ABSTRACT:

The MTU MCFC program is carried out by a European consortium comprising the German

companies MTU Friedrichshafen GmbH, Ruhrgas AG and RWE Energie AG as well as the Danish company

Energi E2 S/A. MTU acts as consortium leader. The company shares a license and technology exchange agreement with Fuel Cell Energy Inc., Danbury, CT, USA (formerly Energy Research Corp., ERC). The program was started in 1990 and covers a period of about 10 years. The highlights of this program to date are: considerable improvements regarding component stability have been demonstrated on laboratory scale; manufacturing technology has been developed to a point which enables the consortium to fabricate the porous components on a 250 cm2 scale. Several large area stacks with 5000-7660 cm2 cell area and a power range of 3-10 kW have been tested at the facilities in Munich (Germany) and Kyndby (Denmark). These stacks have been supplied by FCE; and as far as the system design is concerned it was soon realized that conventional systems do not hold the promise for competitive power plants. A system analysis led to the conclusion that a new innovative design approach is required. As a result the 'Hot Module' system was developed by the consortium. A Hot Module combines all the components of a MCFC system operating at the similar temperatures and pressures into a common thermally insulated vessel. In August 1997 the consortium started its first full size Hot Module MCFC test plant at the facilities of Ruhrgas AG in Dorsten, Germany. The stack was assembled in Munich using 292 cell packages purchased from FCE. The plant is based on the consortium's unique and proprietary 'Hot Module' concept. It operates on pipeline natural gas and was grid connected on 16 August 1997. After a total of 1500 h of operation, the plant was intentionally shut down in a controlled manner in April 1998 for post-test analysis. The Hot Module system concept has demonstrated its functionality. The safety concept has been convincingly proven, though in part unintentionally. The electrical power level of 155 kW (ca. 60% of maximum power) achieved allows validation of the concept with reasonable degree of confidence. Horizontal stack operation-an essential innovation of the Hot Module concept-is feasible. The fuel processing subsystem worked reliably as expected. After initial problems in the inverter control software, the electrical and control subsystem operated to full satisfaction. Stable automatic operation not only under various load conditions, but also in idle mode, hot parking mode, and grid-independent mode has been demonstrated. Together with progress achieved by FCE in the qualification of large direct fuel cell (DFC) stacks the basis was laid for the next test unit of similar design, which will be operated in Bielefeld,

Germany. The pre-tests of the stack took place in July 1999 with good results. Additionally, projects for the test of the DFC Hot Module operating on biogas and other opportunity fuels

are under preparation

CLASSIFICATION CODE: A8630G Fuel cells; B8255 Fuel cell power plants;

B8410G Fuel cells

CONTROLLED TERM: fuel cell power plants;

molten carbonate fuel cells

SUPPLEMENTARY TERM: operating experience; MCFC power plant; molten

> carbonate fuel cell power plant; MTU MCFC program; MTU Friedrichshafen GmbH; Ruhrgas AG; RWE Energie AG; Energi E2 S/A; Fuel Cell Energy

Inc; component stability; manufacturing technology; porous components; Hot Module system; common thermally insulated vessel; Dorsten; pipeline natural gas; safety; electrical power level; horizontal stack

operation; fuel processing subsystem; inverter control software; control subsystem; electrical subsystem; hot parking mode; grid-independent mode; idle mode; load conditions; large direct fuel cell stacks; Bielefeld; Germany; biogas;

250 kW; 1500 h; 155 kW; 3 to 10 kW

power 2.5E+05 W; time 5.4E+06 s; power 1.55E+05 PHYSICAL PROPERTIES:

W; power 3.0E+03 to 1.0E+04 W

ELEMENT TERMS: S; C*T; CT; C cp; cp; T cp

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AUTHOR:

ACCESSION NUMBER: 2003-0083030 PASCAL

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TITLE (IN ENGLISH): Synthesis and characterization of polyaryl blend

membranes having different composition,

different covalent and/or ionical cross-linking

density, and their application to DMFC International congress on membranes

and membrane processes (ICOM),

Toulouse, France, July 7-12, 2002. (Vol.4) KERRES J.; ZHANG W.; ULLRICH A.; TANG C.-M.;

HEIN M.; GOGEL V.; FREY T.; JOERISSEN L.

CORPORATE SOURCE: Institute for Chemical Engineering, University

of Stuttgart, 70199 Stuttgart, Germany, Federal

Republic of

SOURCE: Desalination: (Amsterdam), (2002), 147(1-3),

173-178, 11 refs.

Conference: ICOM: International Congress on Membranes and Membrane Processes, Toulouse

(France), 7 Jul 2002

ISSN: 0011-9164 CODEN: DSLNAH

DOCUMENT TYPE: Journal; Conference

BIBLIOGRAPHIC LEVEL: Analytic

COUNTRY: Netherlands LANGUAGE: English

AVAILABILITY: INIST-12906, 354000104733880290

ABSTRACT: In this contribution, different ionomer blend

membrane types which show high proton

conductivity, thermal

stability, and good direct

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methanol fuel cell
```

(DMFC) performance, are presented: (1) Covalently cross-linked blend membranes from polyaryl sulfinates and polyaryl sulfonates where the sulfmate groups were crosslinked by alkylation with 1,4-diiodobutane; (2) ionically cross-linked blend membranes from polyaryl sulfonates and poly(het)aryl N bases; (3) covalent-ionically cross-linked blend membranes from polyaryl sulfmates, polyaryl sulfonates, and poly(het)aryl N bases; and (4) blend membranes which additionally contain an inorganic compound. The inorganic compound was mixed into the membrane. As aryl polymers, different poly(ethersulfone)s and different poly(etherketone)s have been used, as hetaryl N base, polybenzimidazole PBI Celazole® has been applied. The membrane characterization yielded the following results: (1) high proton conductivities of the membranes could be realized; (2) the TEM micrographs showed that phase-separated or homogeneous morphologies could be realized in the membranes; (3) the DMFC application of the membranes showed that the developed nonfluorinated ionomer membranes have a DMFC performance comparable to perfluorinated ionomer membranes, reaching peak power densities of around 0.25 W/cm.sup.2 at 110°C. It was also found that the addition of SiO.sub.2 powder dramatically reduced the MeOH permeability, but also led to a worse DMFC performance, probably caused by a worse contact membrane-electrode because of a rougher membrane surface caused by the inorganic compound.

CLASSIFICATION CODE:

001D10A06J; Applied sciences; Polymer

technology, Materials science

001D06D03E; Applied sciences; Energy; Thermal

use of fuels 230; Energy

CONTROLLED TERM:

Cation exchange membrane; Ether

copolymer; Ketone copolymer; Sulfonate copolymer; Sulfone copolymer; Aromatic

copolymer; Ionomer; Polymer blends; Crosslinked copolymer; Preparation; Crosslinking; Property composition relationship; Proton conductivity; Transport properties; Liquid permeability;

Methanol; Use; Fuel cell;

Experimental study

BROADER TERM:

Electrical properties

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ACCESSION NUMBER:

2002-0476513 PASCAL

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reserved.

TITLE (IN ENGLISH):

Modified Nafion®-based membranes

for use in direct methanol

fuel cells

Proceedings of the Ringberg Workshop

"Interfacial Kinetics and Electrochemistry", Schloss Ringberg; Tegernsee, Germany, 2000

DIMITROVA P.; FRIEDRICH K. A.; STIMMING U.; VOGT

KOLB Dieter M. (ed.); MAIER Joachim (ed.)

CORPORATE SOURCE: Department of Physics E19, Interfaces and Enemy

> Conversion, Technische Universitdt Muenchen, James-Franck-Strasse 1, 85748 Garching, Germany,

Federal Republic of

University of Ulm, Germany, Federal Republic of;

Max-Planck-Institut fuer Festkorperforchung,

Stuttgart, Germany, Federal Republic of

Solid state ionics, (2002), 150(1-2), 115-122,

Conference: Interfacial Kinetics and

Electrochemistry. Workshop, Tegernsee (Germany,

Federal Republic of), 2000 ISSN: 0167-2738 CODEN: SSIOD3

DOCUMENT TYPE:

BIBLIOGRAPHIC LEVEL:

COUNTRY:

LANGUAGE:

AUTHOR:

SOURCE:

AVAILABILITY:

ABSTRACT:

Journal; Conference

Analytic Netherlands

English

INIST-18305, 354000104526140100 Commercially available Nafion®

membranes at present do not meet the

requirements for high power density

direct methanol fuel

cell (DMFC) applications, amongst others factors because of their high methanol permeability. With the aim of improving the membrane properties with respect to this

application, a modification procedure has been

applied to recast Nafion®-based

membranes. Membranes,

containing different additives namely silicon

dioxide particles (Aerosil®) and

molybdophosphoric acid, are assessed with regard to their conductivity and methanol permeation rate. The preparation of the samples involves the introduction of a small amount of a high boiling point solvent to the as-received Nafion® solution and then shaping the

membranes by a recast procedure. An enhancement of the conductivity of the

thermally treated membranes in

comparison to Nafion® 117 is found. The combined parameter of methanol permeation rate and conductivity of the samples, containing

inorganic additives (Aerosil and

molybdophosphoric acid), decreases compared with

the pure recast and as-received Nafion® membranes. The observed results are discussed in terms of the membrane

structure and preparation.

CLASSIFICATION CODE: 001D06D03E; Applied sciences; Energy; Thermal

> use of fuels 230; Energy

CONTROLLED TERM:

Alcohol fuel cells;

Methanol; Membrane; Permeation;

Composite material; Molybdophosphoric acid;

Ionic conductivity

ANSWER 13 OF 14 PASCAL COPYRIGHT 2007 INIST-CNRS. ALL RIGHTS L52

RESERVED. on STN

2003-0062205 ACCESSION NUMBER: PASCAL

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reserved.

TITLE (IN ENGLISH): A pore-filling electrolyte membrane

-electrode integrated system for a

direct methanol fuel cell application

YAMAGUCHI Takeo; IBE Masaya; NAIR Balagopal N.; **AUTHOR:**

NAKAO Shin-Ichi

CORPORATE SOURCE: Department of Chemical System Engineering, The

University of Tokyo, Bunkyo-ku, Tokyo 113-8656, Japan; Japan Science and Technology Corporation, Kawaguchi, Saitama, Japan; Noritake Company, Limited, Research and Development Center,

Miyoshi, Aichi, Japan

SOURCE: Journal of the Electrochemical Society, (2002),

> 149(11), A1448-A1453, 14 refs. ISSN: 0013-4651 CODEN: JESOAN

DOCUMENT TYPE:

BIBLIOGRAPHIC LEVEL:

COUNTRY: United States

LANGUAGE:

English

INIST-4925, 354000105401450110 AVAILABILITY:

Journal

Analytic

ABSTRACT: To develop a high performance direct

methanol fuel cell,

a novel electrolyte membrane is needed. This electrolyte membrane

should be durable up to 130°C to improve the catalytic reaction, and the methanol

crossover should be reduced. Our approach was to

design a pore-filling-type polyelectrolyte membrane, where the polyelectrolyte is filled into the pores of a porous substrate. This makes an integrated system with a

membrane and a catalyst layer. The

porous substrate was completely inert to aqueous

methanol solution and was durable at high

temperature. The substrate matrix could suppress

membrane swelling to reduce methanol

crossover, and showed mechanical strength at high temperatures. A radical polymerization technique was employed to fabricate the pore-filling membrane. A porous silica sol-gel thin base membrane on a carbon

electrode was used as a membrane

-electrode integrated system. The substrate

pores were filled with a poly(acrylic acid-co-vinyl sulfonic acid) network. The

membranes showed high proton

conductivity, thermal

stability, and low methanol permeation. 001D06D03E; Applied sciences; Energy; Thermal CLASSIFICATION CODE:

use of fuels

230; Energy .

CONTROLLED TERM: Alcohol fuel cells; Carbon

electrode; Porous electrode; Polymer
electrolytes; Polymeric membrane;

Polyelectrolyte; Sulfonate polymer; Acrylic acid

polymer; Benzene(divinyl) polymer;

Electrochemical properties; Ionic conductivity;

Performance evaluation

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ACCESSION NUMBER: 2000-0278685 PASCAL

TITLE (IN ENGLISH): Inorgano-organic proton conducting

membranes for fuel

cells and sensors at medium

temperatures

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Layered zirconium sulfoarylphosphonates of the

 α - and the γ -type are proton conductors thermally stable up

to at least 180 °C. In these materials,

the sulfophenyl groups are bonded through the

phosphorus atoms to an α - or a

 γ -inorganic framework made of oxygen and zirconium atoms. Compounds where the sulfonic function is attached to a phenyl, benzyl or to a fluorinated benzyl group were characterized for their conductivity as a function of temperature and relative humidity (r.h.). Independent of the layer type, the highest conductivities were found for the sulfophenylphosphonates. The

conductivity is strongly affected by the r.h. reaching values of 5 x 10-2 S cm-1 at 100 °C (100% r.h.) and 2 x 10-2 S cm-1 at 150 °C (80% r.h.). Due to their ability to undergo infinite swelling in appropriate solvents, these materials can be incorporated

into polymeric proton conducting membranes. The possible advantages of these membranes for increasing the efficiency of indirect or direct

methanol fuel cells

working at medium temperature are discussed. The

use of these **membranes** in gas sensors working at medium temperatures are also

discussed. Preliminary results for the detection

of hydrocarbons at 300 °C by means of a sensor based on the protonic conductivity of

zirconium phosphate are reported.

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